



Carbon modified porous γ -Fe₂O₃ as anode for high performance Li-ion batteries

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Abstract

Carbon modified porous γ -Fe₂O₃ particles (PFe₂O₃-C) are synthesized by a high temperature calcination method using sodium chloride as a template. During the nucleation and carbonation process, the Fe(NO₃)₃-C₁₀H₁₅N₅ complex uniformly dispersed on the surface of NaCl particles which can limit its longitudinal growth, thus forming independent and homogeneous nanoparticles with a diameter of about 30 nm. Because of this special structure, the γ -Fe₂O₃ particles have a sufficient interspace between them, which can not only provide a large number of active sites for storing lithium ions, but also shorten diffusion length for lithium ion transport. The introduction of carbon can offer additional lithium ion storage and improve overall electrical conductivity. This PFe₂O₃-C electrode exhibits excellent rate performance (1139, 1067, and 972 mAh g⁻¹ at 2, 5, and 10 C, respectively, 1 C = 924 mAh g⁻¹) and cycle performance (up to 2100 mAh g⁻¹ after 200 cycles at 0.3 C).

1 Introduction

Lithium-ion batteries (LIBs) play an important role in energy storage devices due to their extraordinary properties, such as long cycle life, high work voltage, no memory effect and environment-friendliness [1–3]. However, energy density and power density of LIBs still cannot satisfy the ever-increasing demands of electric vehicles and portable electronics [4, 5]. In principle, the energy storage is mainly achieved through the reversible conversion reaction in the electrode materials, which is the key factor to determine the performance of LIBs [2]. Therefore, exploring new anode materials to replace commercial graphite anode, which exhibits low theoretical capacity of 372 mAh g⁻¹, has aroused great concern [6].

In recent years, transition metal oxides (TMOs) gain increasing interest because of their high theoretical capacity

(450–1500 mAh g⁻¹) and high abundance [3, 7]. Among these materials, Fe₂O₃ attracts more attentions due to its extraordinary properties, including high theoretical capacity (1007 mAh g⁻¹), low cost, non-toxicity, high corrosion resistance and easy to exploit [8–11]. Unfortunately, due to its poor intrinsic electronic conductivity and huge volume variation during the repeated lithiation/delithiation process, Fe₂O₃ electrode has high irreversible capacity loss, low initial coulombic efficiency and cycling stability, which has been hindering its commercial applications in LIBs [9, 12].

To overcome these drawbacks, many approaches have been exploited and could be classified into two groups. One of them is the construction of a porous architecture, which can not only withstand large volume changes caused by Li⁺ insertion/extraction but also provide more active sites for storing lithium ions and effective paths for transferring lithium ion and electron [13–17]. Another one is the surface modification of TMOs nanostructure with carbonaceous materials to improve electrical conductivity as well as provide additional capacity [3, 8, 18–21]. Carbonaceous materials formed from different carbon precursors have different structural and electrochemical properties. Among these carbon precursors, ionic liquids (ILs) are gaining more and more attention because of their outstanding characteristics such as low viscosity, good fluidity, low vapor pressure and good thermal stability. Therefore, carbonaceous materials derived from ILs have a higher electrical conductivity and bonding strength [22].

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In this work, we used sodium chloride as a template to synthesize $\text{PFe}_2\text{O}_3\text{-C}$ at high temperatures. The produced $\text{PFe}_2\text{O}_3\text{-C}$ is consisted of independent and homogeneous $\gamma\text{-Fe}_2\text{O}_3$ nanoparticles with a diameter of ~ 30 nm. When served as an anode material for LIBs, $\text{PFe}_2\text{O}_3\text{-C}$ exhibits high specific capacity and remarkable rate capability. It was also found that the increase of capacity is mainly occurred below 0.61 V due to the growth of polymeric gel-like film.

2 Experimental section

2.1 Synthesis of $\text{PFe}_2\text{O}_3\text{-C}$

The reagents were obtained from commercial suppliers and used without further purification. In a typical process, $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ (1.81 g), 1-butyl-3-methylimidazolium dicyanamide ([BMIm][N(CN)₂]) (1.28 g), and NaCl (18 g) were first dissolved in 35 mL deionized water. The solution was then dried in a drying oven at 80 °C for 24 h. After that, the obtained materials were annealed at 760 °C for 2 h in a tube furnace in flowing argon atmosphere to obtain carbon-modified Fe nanoparticles coated on the NaCl particles (Fe-C@NaCl). In the second step, the Fe-C@NaCl nanoparticles were heated at 260 °C for 6 h in air to oxidize the Fe to yield carbon-modified $\gamma\text{-Fe}_2\text{O}_3$ nanoparticles coated on the NaCl particles ($\text{PFe}_2\text{O}_3\text{-C@NaCl}$). After cooling to room temperature, the obtained powder was washed with deionized water to dissolve the NaCl and $\text{PFe}_2\text{O}_3\text{-C}$ was obtained. For comparison, $\text{Fe}_2\text{O}_3\text{-C}$ composites were also synthesized by carbonizing the mixture of $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ and [BMIm][N(CN)₂] without NaCl under the same conditions.

2.2 Structural and morphology characterization

The X-ray powder diffraction (XRD) patterns of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$, $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ were collected by using a Rigaku D/max-2500 with Cu K α radiation. Transmission electron microscopy (TEM) characterizations were carried out with a JEOL JEM-2010F equipment. The morphologies of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$, $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ were observed on field emission scanning electron microscope (FESEM) by using an acceleration voltage of 15 kV (tescan MIRA3). Raman spectra of the samples were recorded on LabRAM-HR800. Nitrogen adsorption and desorption isotherms was performed on Quadrasorb SI. The surface area and pore size distribution of samples were calculated by BET and DJH method, respectively. The total pore volume was calculated by the adsorption amount of nitrogen at relative pressure (P/P_0) of 0.99.

2.3 Electrochemical measurement

The electrochemical measurements of the anode materials were carried out in a half coin-type cell. The coating slurry is prepared by mixing 70 wt% active material, 20 wt% Super P, and 10 wt% polyvinylidene fluoride in *N*-methyl pyrrolidone. The solvent was evaporated on a copper foil at 80 °C for 12 h. A lithium foil served as counter electrode and was separated from the work electrode with the Celgard 2400 micro-porous polypropylene film. The electrolyte is a solution of 1 M lithium hexafluorophosphate (LiPF₆) that dissolved in the mixture of ethylene carbonate (EC) and 1,2-dimethoxyethane (DME) with a volume ratio of 1:1. The cycle performance and rate capability were performed in the voltage range between 0.001 and 3.0 V (vs. Li/Li⁺) on a battery test system (LAND CT2001, China). Electrochemical impedance spectra (EIS) and cyclic voltammetry (CV) measurements were performed at room temperature on a CHI660D electrochemistry workstation (Chenhua, China).

3 Result and discussion

Figure 1 shows the XRD patterns of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$, $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$. For $\text{PFe}_2\text{O}_3\text{-C@NaCl}$ samples, the diffraction peaks at 27.3°, 31.6°, 45.3°, 53.7°, 56.3°, 66.1°, 72.92°, 75.1° and 83.8° are assigned to (111), (200), (220), (311), (222), (400), (331), (420) and (422) planes of NaCl (JCPDS No 70-2509), respectively. The diffraction peak of $\gamma\text{-Fe}_2\text{O}_3$ was less obvious, which may be attributed to the low content of $\gamma\text{-Fe}_2\text{O}_3$ in $\text{PFe}_2\text{O}_3\text{-C@NaCl}$ [23]. For $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$, all diffraction peaks well correspond to the planes of maghemite $\gamma\text{-Fe}_2\text{O}_3$ (JCPDS No 39-1346) [8, 24]. Sharp diffraction peaks indicate good crystallinity of both samples. No other diffraction peak was observed, indicating that no other polymorphs iron oxide generation [25]. From previous literature, it can be known that the $\gamma\text{-Fe}_2\text{O}_3$ will not be further oxidized during the cycle [26]. The diffraction peak of carbon was not observed, which may be due to the low content of carbon $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$. XRD results indicate that $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ materials were successfully prepared [27].

SEM and TEM are used to analyze the morphologies of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$, $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ materials. From Fig. 2a–c, we can see that the $\text{PFe}_2\text{O}_3\text{-C}$ uniformly dispersed on the surface of NaCl particles. The addition of NaCl can limit the longitudinal growth of the $\text{Fe}(\text{NO}_3)_3\text{-C}_{10}\text{H}_{15}\text{N}_5$ complex in nucleation and carbonation process, which result in independent and

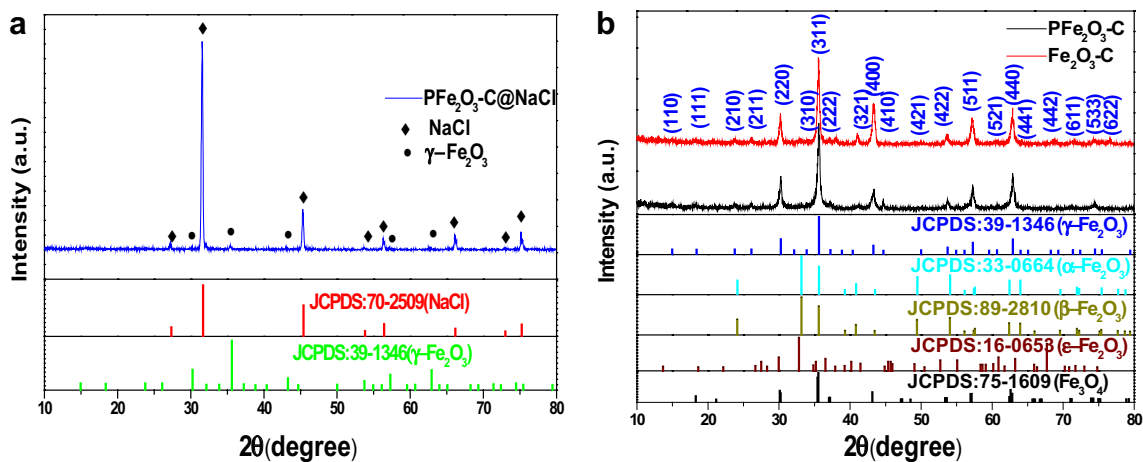


Fig. 1 XRD patterns of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$ (a), $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ (b)

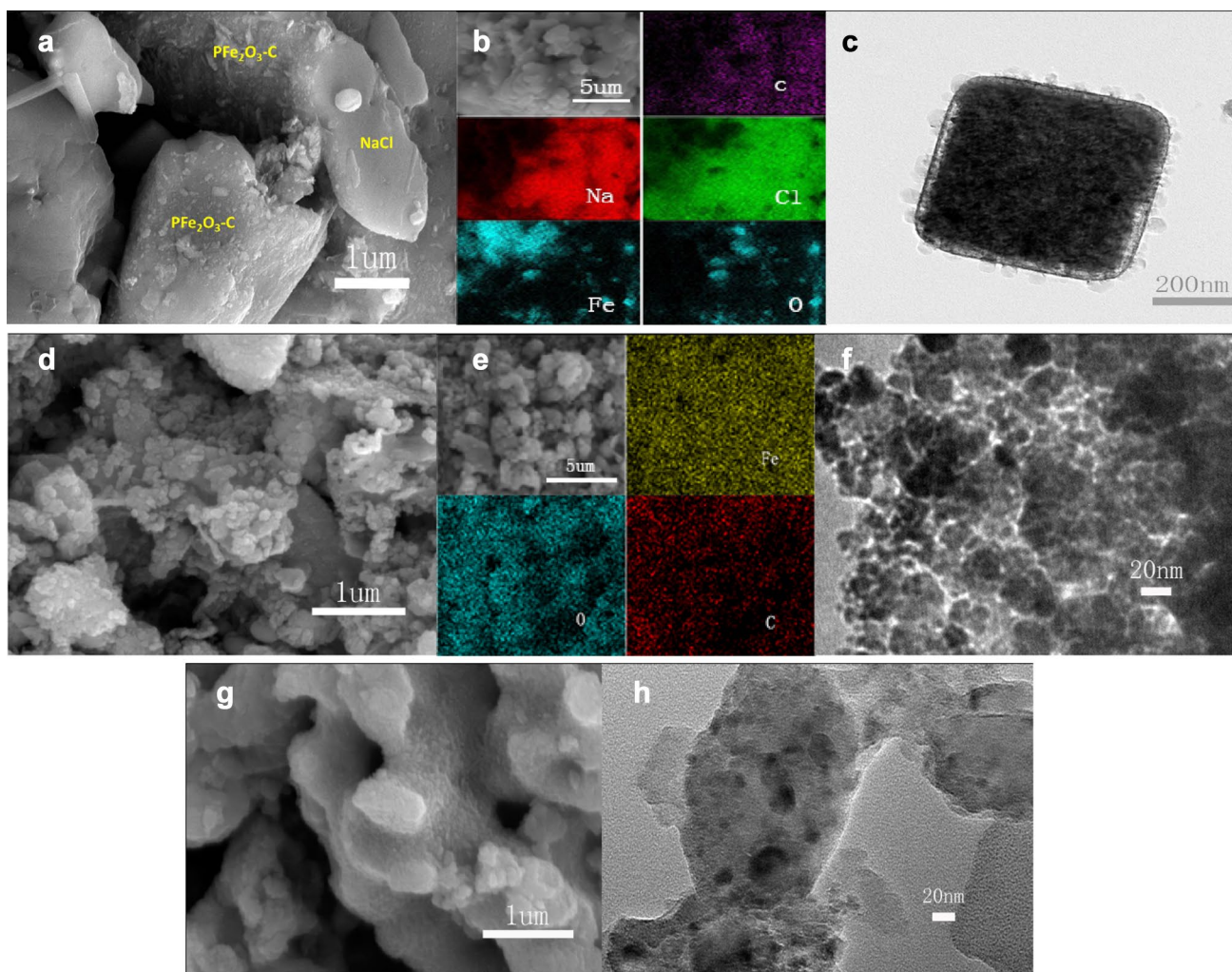


Fig. 2 a SEM image, b EDS elemental mapping, and c TEM image of $\text{PFe}_2\text{O}_3\text{-C@NaCl}$; d SEM image, e EDS elemental mapping, and f TEM image of $\text{PFe}_2\text{O}_3\text{-C}$; g SEM image and h TEM image of $\text{Fe}_2\text{O}_3\text{-C}$

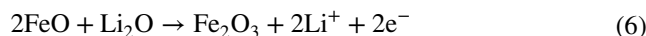
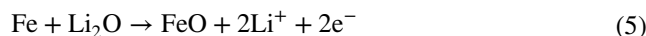
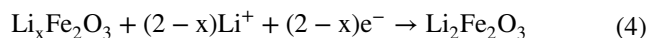
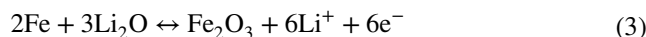
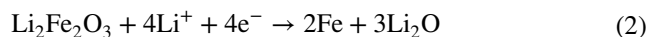
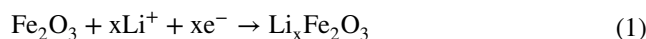
homogeneous nanoparticles with a diameter of ~ 30 nm. As can be seen from Fig. 2d, PFe₂O₃-C material has rough surfaces and the nanoparticles have a diameter of about 30 nm. While the surface of Fe₂O₃-C is smooth and the Fe₂O₃ particles have a large diameter of ~ 500 nm (Fig. 2g, h). The result of EDS elemental analysis show the uniform distribution of carbon on the Fe₂O₃ particles, which can provide additional sites for lithium ion storage and improve the electrical conductivity (Fig. 2e). The TEM image (Fig. 2f) further confirms that PFe₂O₃-C consists of independent and homogeneous nanoparticles that are separated by significant gap. This unique structure can shorten the lithium-ion and electron transport path, buffer the lithium-ion volume expansion, and provide more active sites. In comparison, the Fe₂O₃-C material in Fig. 2g, h consists of bulk particles with no obvious boundaries between the particles. This structure cannot facilitate lithium ion transport or buffer the volume expansion [28].

To further study the structure of carbon in the PFe₂O₃-C and Fe₂O₃-C, the Raman spectroscopy was applied. In Fig. 3a, the two broad Raman bands at about 1342 and 1586 cm⁻¹ correspond to the D-band of edge and disordered structures and the ordered sp²-hybridized G-band, respectively [29]. The intensity ratio of D band to G band (I_D/I_G) is indicator of the crystallinity of various carbon materials. The larger value of I_D/I_G , the higher the degree of disorder in the carbon material [30]. The I_D/I_G ratios of PFe₂O₃-C and Fe₂O₃-C were 1.22 and 1.13, respectively, indicating that PFe₂O₃-C has more defects and lower ordered structure, which can provide more active sites for lithium ion storage, thus contributing extra specific capacity. Three large bands at 700 cm⁻¹ (A₁), 500 cm⁻¹ (E) and 350 cm⁻¹ (T₁) attributed to the vibration modes of γ -Fe₂O₃, further confirming that Fe element was completely oxidized to γ -Fe₂O₃ [31].

N₂ adsorption-desorption isotherms of PFe₂O₃-C and Fe₂O₃-C are shown in Fig. 3b. The isothermal curves of

both samples exhibit a type IV curve with H3 hysteresis loop located at a relative pressure of 0.4–1.0. The pore size distribution (inset in Fig. 3b) indicates that PFe₂O₃-C has more micropores and mesopores [32, 33]. The specific surface area of PFe₂O₃-C (26.9 m² g⁻¹) is about four times of Fe₂O₃-C (6.7 m² g⁻¹), which can provide more active sites for the storage of lithium ions and serve as an effective electron transport path [34]. The pore volume of PFe₂O₃-C (about 0.072 cm³ g⁻¹) is also much larger than Fe₂O₃-C (about 0.021 cm³ g⁻¹). Therefore, PFe₂O₃-C has better performance on buffering the volume change of the Fe₂O₃ nanocrystal during charge/discharge cycles. This is consistent with the results of TEM and SEM.

Figure 4a shows the CV plots of PFe₂O₃-C electrode for four cycles at a scan rate of 0.1 mV s⁻¹ from 0 to 3.0 V (vs. Li/Li⁺). These plots display a typical pattern of Fe₂O₃-C composite [35, 36]. The electrochemical reaction of Li⁺ with Fe₂O₃ can be described by the following equations [37–40]:



In the first cathode curve, the peak at 0.97 V is related to the lithium intercalation into the γ -Fe₂O₃ crystal structure (Eq. 1). The capacity associated with the voltage drop is 267 mAh g⁻¹ (Fig. 4b), which is equivalent to the uptake of 1.6 mol of Li ($x=1.6$, in Eq. 1) per mole of PFe₂O₃-C. Thus, the above steps generate the Li_{1.6}Fe₂O₃ intermediate product, indicating that the crystal structure of γ -Fe₂O₃

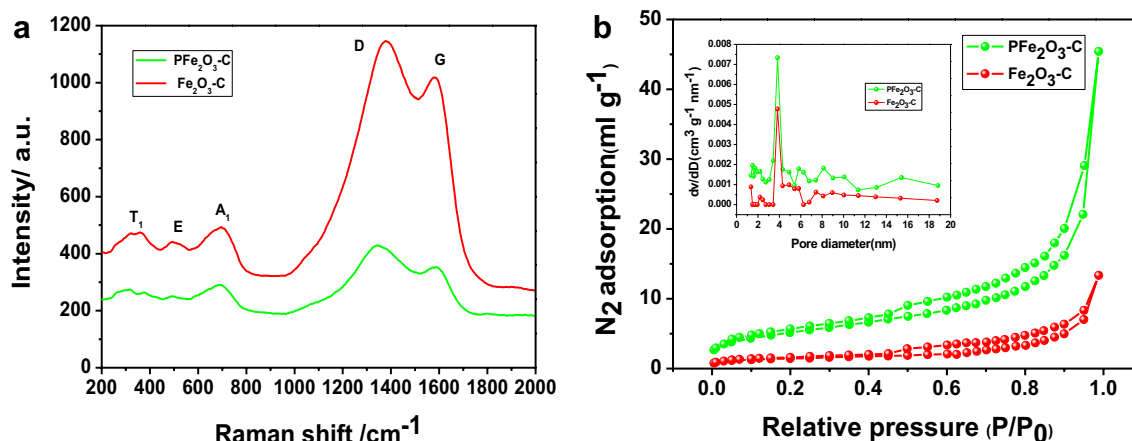


Fig. 3 a Raman spectra, b N₂ adsorption-desorption isotherms and the pore size distribution curves of PFe₂O₃-C and Fe₂O₃-C

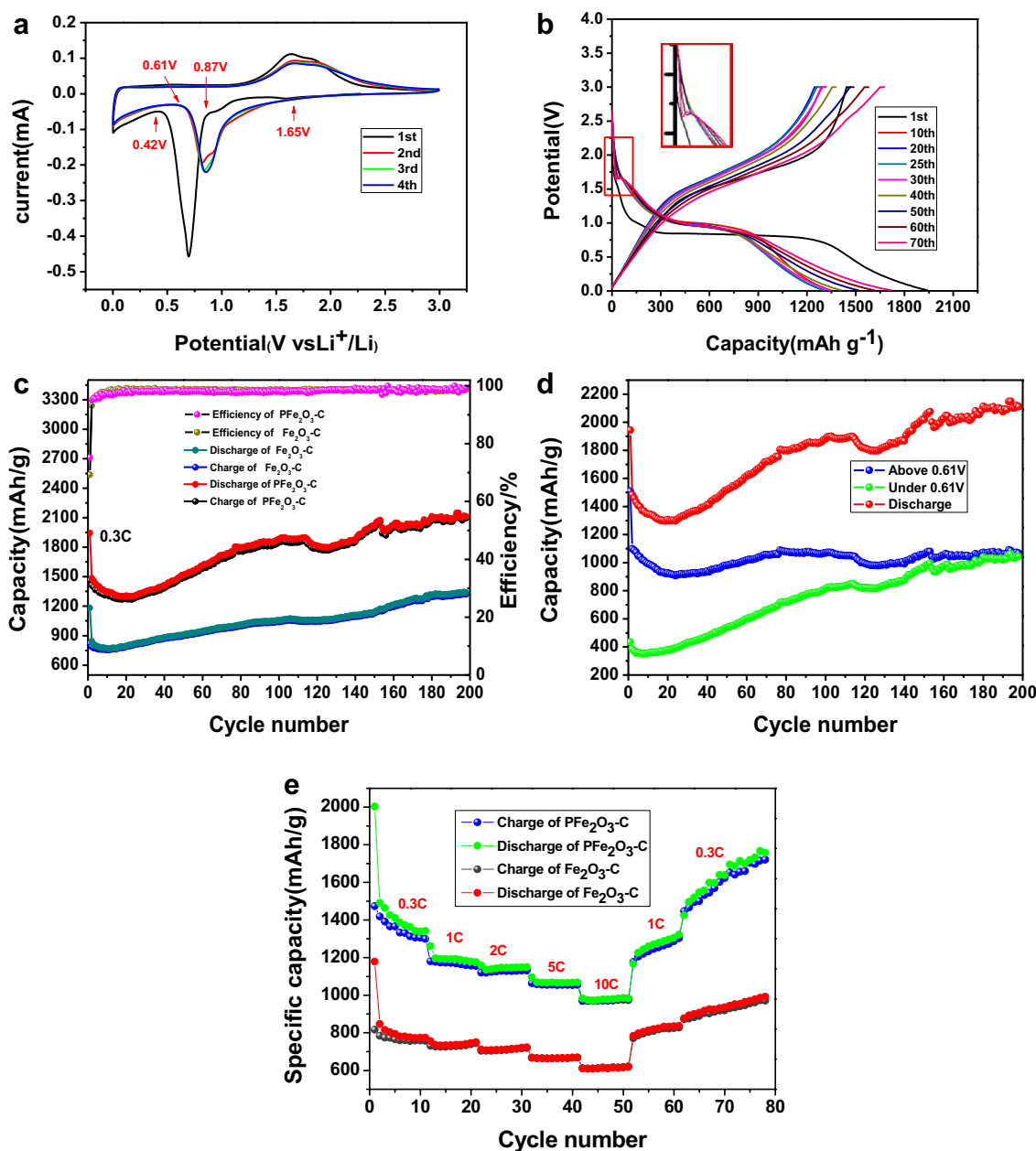


Fig. 4 **a** CV plot of $\text{PFe}_2\text{O}_3\text{-C}$, **b** voltage profiles of $\text{PFe}_2\text{O}_3\text{-C}$, **c** cycle performances of $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ at the current density of 0.3 C in 0.01–3.00 V, **d** schematic illustrations of two parts of bat-

tery capacity of $\text{PFe}_2\text{O}_3\text{-C}$ at 0.3 C between 0.01 and 3 V, and **e** rate capability of $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$. (Color figure online)

is not destroyed [37]. The peak at 0.69 V results from the conversion of $\text{Li}_{1.6}\text{Fe}_2\text{O}_3$ to $\text{Li}_2\text{Fe}_2\text{O}_3$ (Eq. 4, consumed $2-x=0.4$ mol of Li^+), the reduction of Fe^{3+} to Fe^0 (Eq. 2, consumed 4 mol Li^+), and the formation of solid electrolyte interface (SEI) film. It is noteworthy that this peak is vanished at 0.42 V in the first cycle and 0.61 V in the following cycles. The capacity of 1508 mAh g^{-1} is achieved from the open circuit voltage (OCV) to the 0.42 V, representing a total uptake of 9 mol Li^+ per mole of $\text{PFe}_2\text{O}_3\text{-C}$, which corresponds to a complete reduction of Fe^{3+} to Fe^0 (including

Eqs. 1, 2, 4) and SEI film. Obviously, 3 mol Li^+ is consumed to form SEI via subtraction. The total discharge capacity in the first cycle finally reached $1943.8 \text{ mAh g}^{-1}$, which is equivalent to the uptake of 11.6 mol of Li^+ . Therefore, the proportion of Li^+ to form SEI is 25.9%, which is in agreement with the initial coulombic efficiency of 75.2% from voltage profiles of $\text{PFe}_2\text{O}_3\text{-C}$ in Fig. 4b. Another two anodic peaks at 1.63 and 1.83 V are attributed to the oxidation of Fe^0 to Fe^{2+} and Fe^{3+} (Eqs. 5, 6), respectively. In the subsequent cycles, the shift of the main cathode peak from 0.69 to

0.82 V derives from the small scale structural adjustment of $\text{PFe}_2\text{O}_3\text{-C}$, which enhances the electrical contact among the cell components [41]. Starting from the second cycle, the peak position and shape of the CV almost overlap, indicating that the electrode has great reversibility and integrity [42].

Figure 4b shows the voltage profiles of $\text{PFe}_2\text{O}_3\text{-C}$ at the 1st, 10th, 20th, 25th, 30th, 40th, 50th, 60th, and 70th cycles at a current density of 0.3 C. The first discharge and charge capacity are 1943.8 and 1462.1 mAh g^{-1} , respectively. The irreversible capacity loss is due to the formation of SEI film and electrolyte decomposition, resulting in a coulombic efficiency of only 75.22% [43–45]. The discharge voltage plateau at 0.82 V in the first cycle is different from those of other cycles at 0.93 V, indicating that irreversible reactions occurred in the first cycle, which is consistent with the CV results. The discharge curves below 0.61 V become higher and more sloping with the increase of cycle number, indicating that the growth of PGF tended to be easier due to the nanocrystallization of the particles during the repeated lithiation/delithiation process. Interestingly, after 25 cycles, a slight plateau appears at 1.6 V, becoming more obvious as charge/discharge cycles increase, even forming a semicircle at 70 cycles. The main reason is that the stable PGF generated on the surface of the active substance increases the diffusion distance and the resistance of Li^+ . Meanwhile, the charging curve is a sloping curve with no obvious voltage platform, owing to the large surface area induced during the former discharge process which could widen the reaction site energy range for intercalation compound or the amorphous character of the active materials itself.

Figure 4c shows the long cycling performance of $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ at a current density of 0.3 C. The reversible capacity of $\text{PFe}_2\text{O}_3\text{-C}$ retains to 1306 mAh g^{-1} after 20 cycles and increases to 1881 mAh g^{-1} after 100 cycles. The capacity fading of $\text{PFe}_2\text{O}_3\text{-C}$ electrode in the preliminary cycles is due to the decomposition of the SEI film on the Fe_2O_3 -based anode surface. According to the SEM and BET results, the $\text{PFe}_2\text{O}_3\text{-C}$ electrode has a larger specific surface area than $\text{Fe}_2\text{O}_3\text{-C}$, thus requiring ten more cycles to form the SEI film before terminating by insulate SEI. Subsequent increase in cycle capacity is due to the extra capacity resulting from the reversible formation/decomposition of the polymeric gel-like film (PGF) on the active material surface [46]. This phenomenon has also been found in Fe_3O_4 and many other nanostructured metal oxide anodes [47–50]. Due to the high specific surface area of $\text{PFe}_2\text{O}_3\text{-C}$, more PGF can be grown on the surface of the active material, leading to larger capacity increase of $\text{PFe}_2\text{O}_3\text{-C}$ than $\text{Fe}_2\text{O}_3\text{-C}$.

To study the behavior of the discharge capacity (red curve) in each voltage range, the curves are split into two parts: above 0.61 V and below 0.61 V, as shown in Fig. 4d. The blue curve represents the capacity above 0.61 V and the

green curve stands for the capacity below 0.61 V. The blue curve decreases gradually before 20 cycles, which is parallel to the red curve. After 20 cycles, the blue curve remains relatively stable. While the green curve increases after the 10th cycle, and then follows the trend of the red curve after 20 cycles. This indicates that the increased capacity mainly occurs in the region below 0.61 V, which is due to the PGF growth and the fast decomposition of electrolyte at low potentials [51].

In addition to excellent reversible capacity, $\text{PFe}_2\text{O}_3\text{-C}$ also exhibits outstanding rate performance. As shown in Fig. 4e, the rate capacity test was measured on a duplicate cell at different current rates of 0.3, 1, 2, 5, and 10 C in the voltage range of 0.01–3.0 V. The average reversible capacity of $\text{PFe}_2\text{O}_3\text{-C}$ electrode are 1427, 1193, 1139, 1067, and 972 mAh g^{-1} at 0.3, 1, 2, 5, and 10 C, respectively, which are significantly better than the $\text{Fe}_2\text{O}_3\text{-C}$ electrode. The $\text{PFe}_2\text{O}_3\text{-C}$ electrode still provides a higher reversible capacity of 972 mAh g^{-1} even at a high current density of 10 C, corresponding to ~68.1% of the capacity at 0.3 C. When returning to 0.3 C, the reversible capacity of both samples increased in subsequent cycles, which is similar to the cycling performance in Fig. 4c.

The dynamic behavior of $\text{PFe}_2\text{O}_3\text{-C}$ and $\text{Fe}_2\text{O}_3\text{-C}$ was investigated by EIS, as shown in Fig. 5a. The semicircular diameter of $\text{PFe}_2\text{O}_3\text{-C}$ is smaller than that of $\text{Fe}_2\text{O}_3\text{-C}$, indicating that the charge-transfer resistance of $\text{PFe}_2\text{O}_3\text{-C}$ is small. To further study the PGF growth, the EIS of another duplicate at 10th, 20th, 30th, 40th, 50th, 84th and 99th cycles was measured at 1 C, as show in Fig. 5b. The impedance data is analyzed by fitting the equivalent circuit (inset of Fig. 5b), where R_0 , R_f , and R_d represent the electrolyte resistance, the surface film resistance, and the charge transfer resistance, respectively. C_f and C_d are the corresponding capacitances of R_f and R_d , respectively. Therefore, the electronic component groups of Part f (R_f , C_f) and Part d (R_d , C_d) are related to the SEI layer and PGF, respectively. The fitted result for charge transfer resistance (R_d) is shown in Table 1. The value of R_d decreased in the first 30 cycles and increased in subsequent cycles, which is consistent with the capacity behavior. This is due to that a small amount of PGF is generated before the first 30 cycles and more PGF is grown after 30 cycles during charge–discharge process, thereby consuming more Li^+ . This result further explains why the voltage platform appears at ~1.6 V (Fig. 4b).

4 Conclusions

$\text{PFe}_2\text{O}_3\text{-C}$ particles were synthesized by using sodium chloride as a templating agent. Compared with $\text{Fe}_2\text{O}_3\text{-C}$, $\text{PFe}_2\text{O}_3\text{-C}$ consists of uniform and independent Fe_2O_3 nanoparticles with a diameter of about 30 nm, delivering

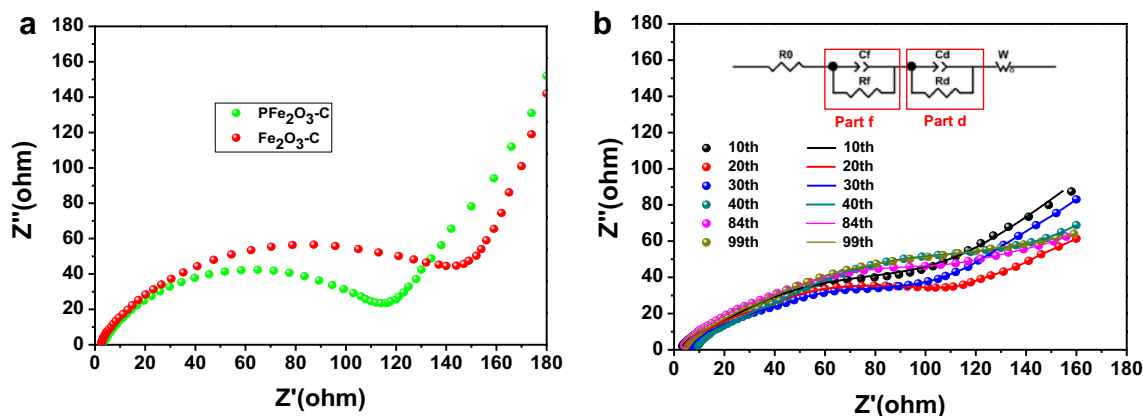


Fig. 5 **a** EIS of PFe₂O₃-C and Fe₂O₃-C before CV. **b** Nyquist plots of PFe₂O₃-C at fully charge stage upon cycles (equivalent electrical circuit in inset)

Table 1 The parameters obtained by fitting an equivalent circuit of PFe₂O₃-C electrodes

Cycle number	10	20	30	40	84	99
Rd (Ω)	78.9	74.2	66.8	86.2	104.2	124.9

high rate capability and cycling performance. This can be attributed porous structure of PFe₂O₃-C, which can provide sufficient active sites for storing lithium ions, shorten the diffusion length and buffer the volume expansion. In addition, integration of carbon can also offer additional lithium ion storage and improve the electrical conductivity of the material. These results indicate this method can be applied to prepare electrode materials for highly efficient energy storage applications, which with further optimization should be suitable for widespread applications.

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